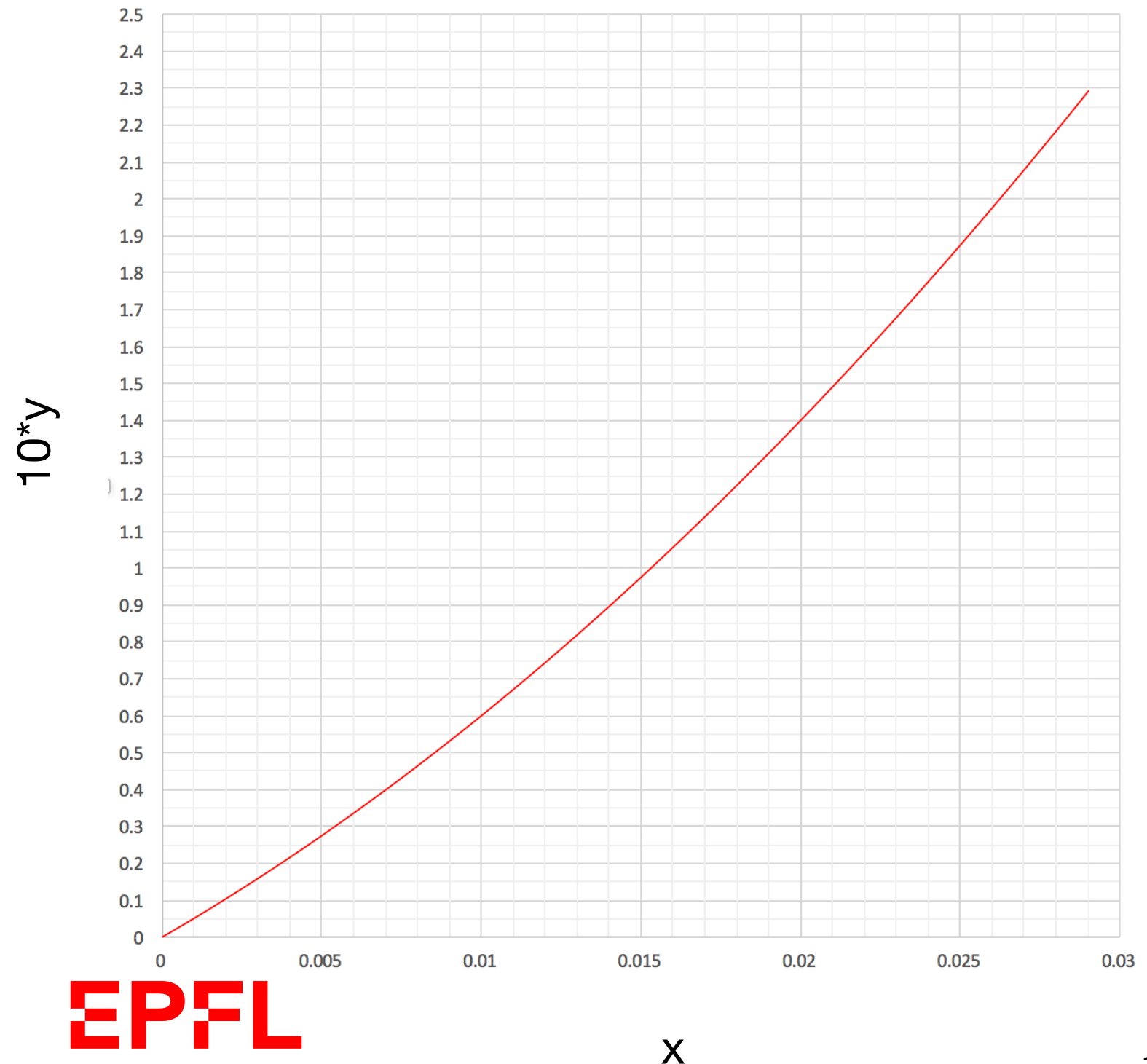
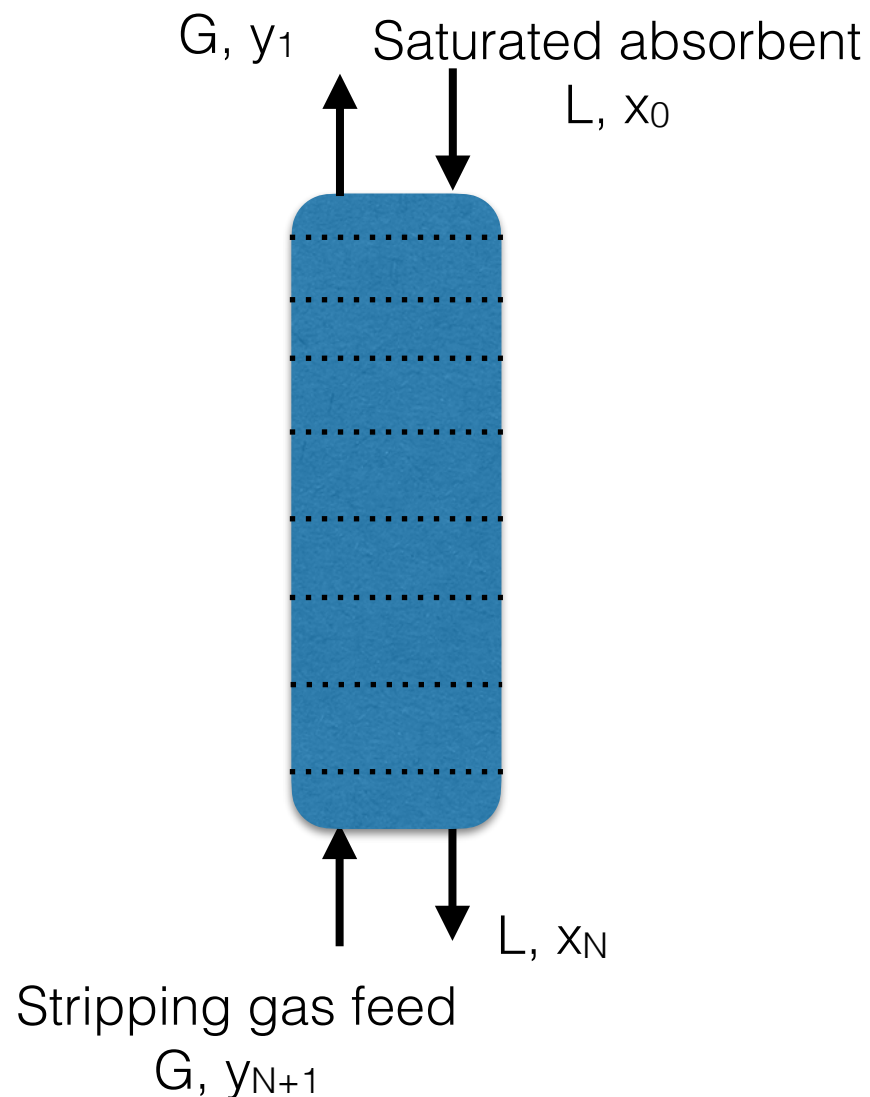


Exercise problem 1: Stripping

100 mol/hr of amine containing 2.9% CO₂ at 1 bar is to be regenerated with steam such that concentration of CO₂ reduces to 1%. Pure steam is being used as the stripping gas. Calculate number of stages if $L/G = 0.5 L/G_{\min}$. Calculate exit concentration of steam.

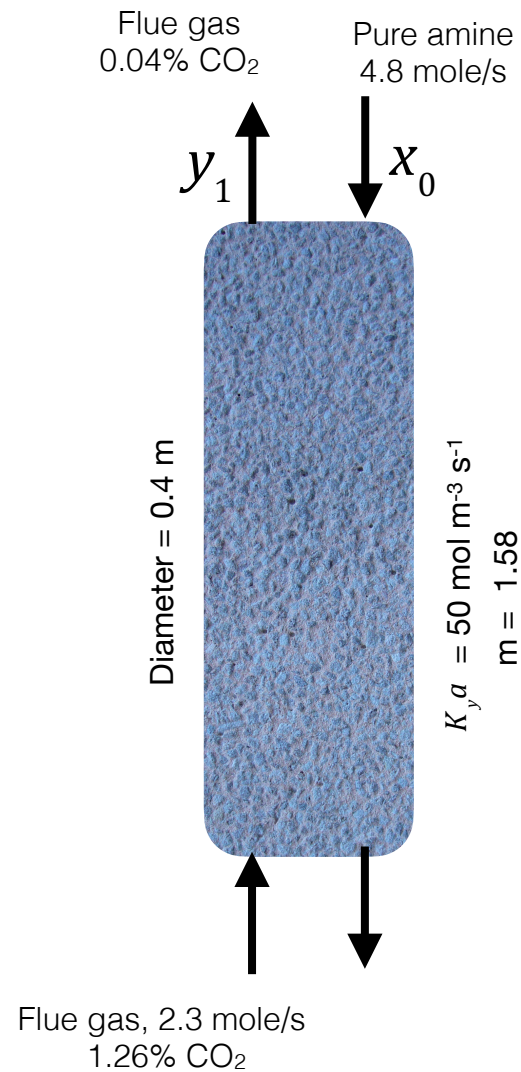
$$y = \frac{L}{G}x + (y_1 - \frac{L}{G}x_0)$$



Exercise problem 2: CO₂ absorption in a packed bed.

Calculate HTU, NTU, and h for the following problem. How would you decrease HTU?

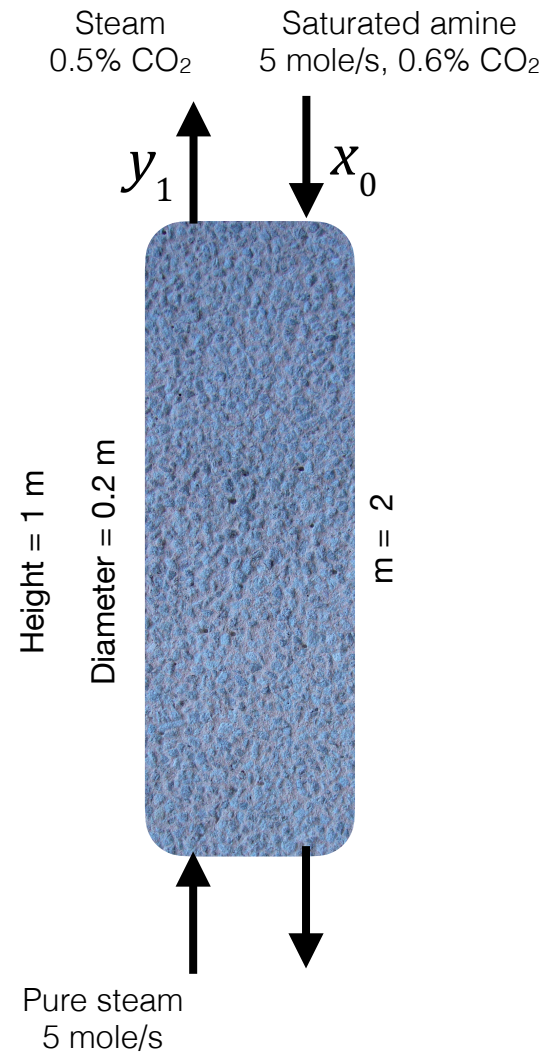
$$h = \frac{G}{K_y a A} \left[\left(\frac{1}{1 - \frac{mG}{L}} \right) \ln \left(\frac{y_{N+1} - m x_N}{y_1 - m x_0} \right) \right]$$



Exercise problem 3: CO₂ stripping in a packed bed.

Calculate HTU, NTU, and K_{ya} for the following problem.

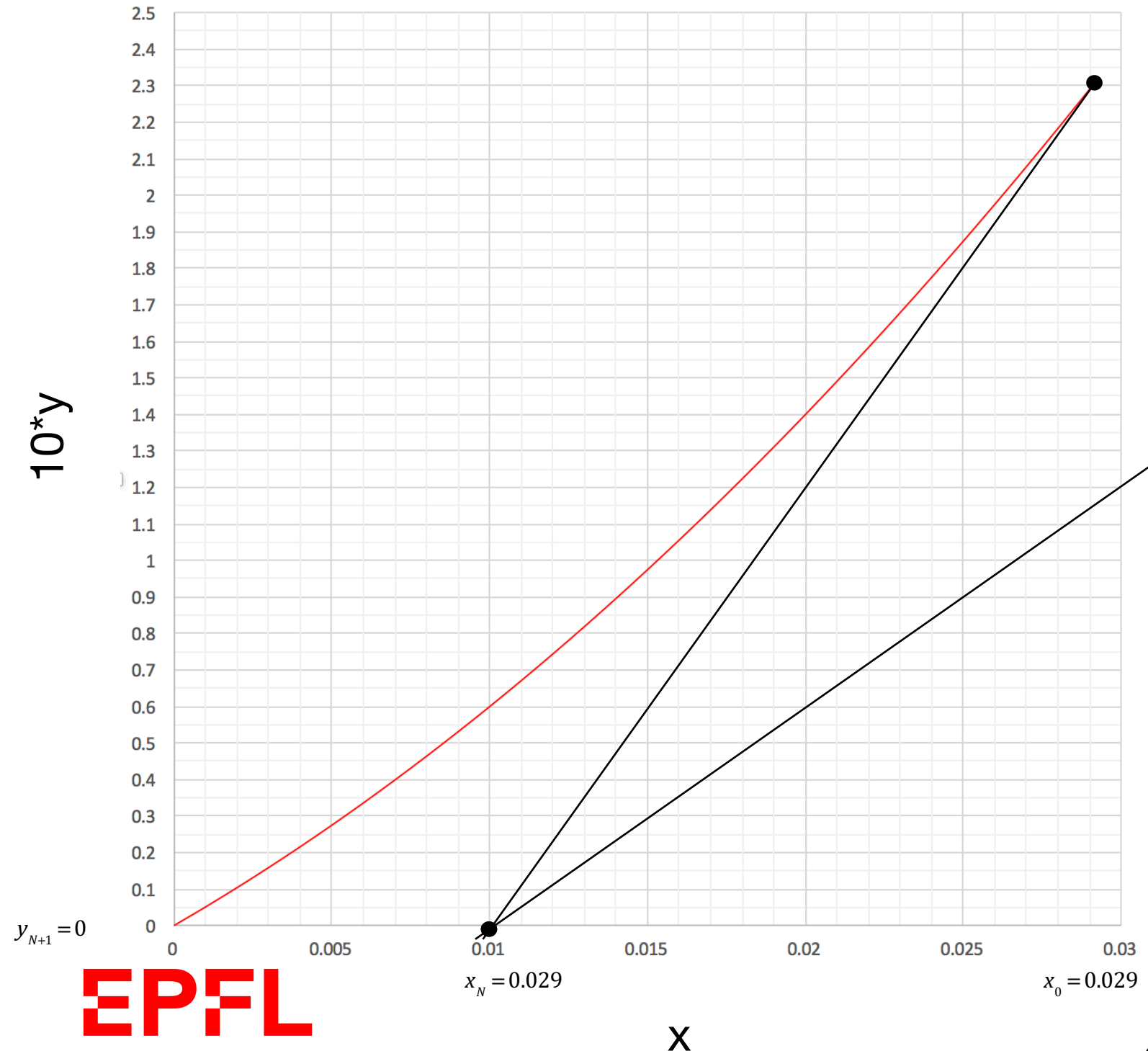
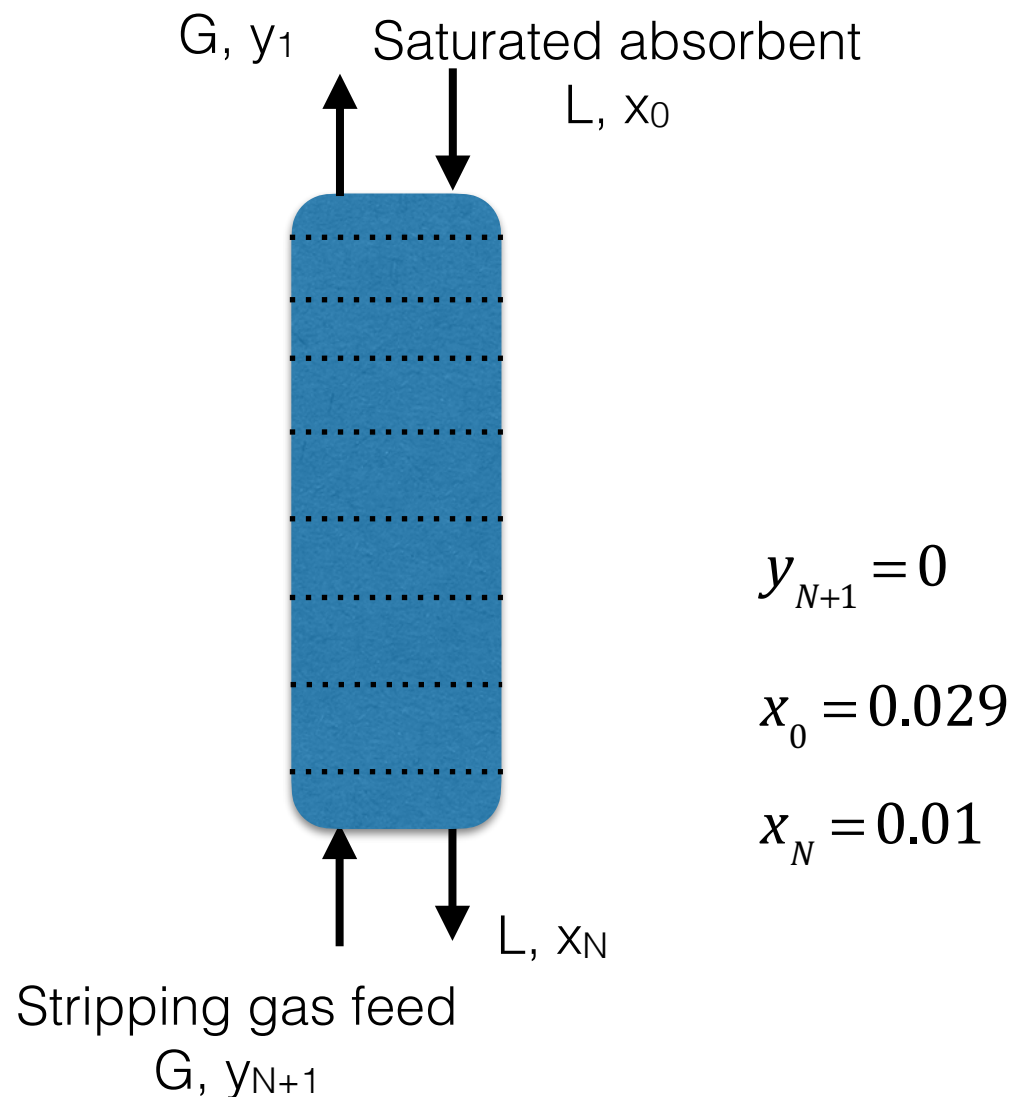
$$h = \frac{G}{K_y a A} \left[\left(\frac{1}{1 - \frac{mG}{L}} \right) \ln \left(\frac{y_{N+1} - m x_N}{y_1 - m x_0} \right) \right]$$



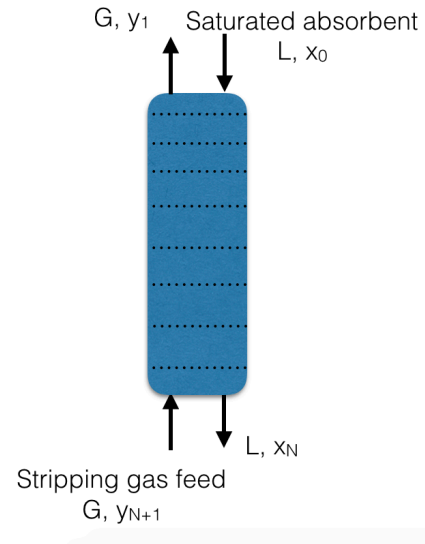
Solution to exercise problem 1

100 mol/hr of amine containing 2.9% CO₂ at 1 bar is to be regenerated with steam such that concentration of CO₂ reduces to 1%. Pure steam is being used as the stripping gas. Calculate number of stages if $L/G = 0.5 L/G_{\min}$. Calculate exit concentration of steam.

$$y = \frac{L}{G}x + (y_1 - \frac{L}{G}x_0)$$



Solution to exercise problem 1

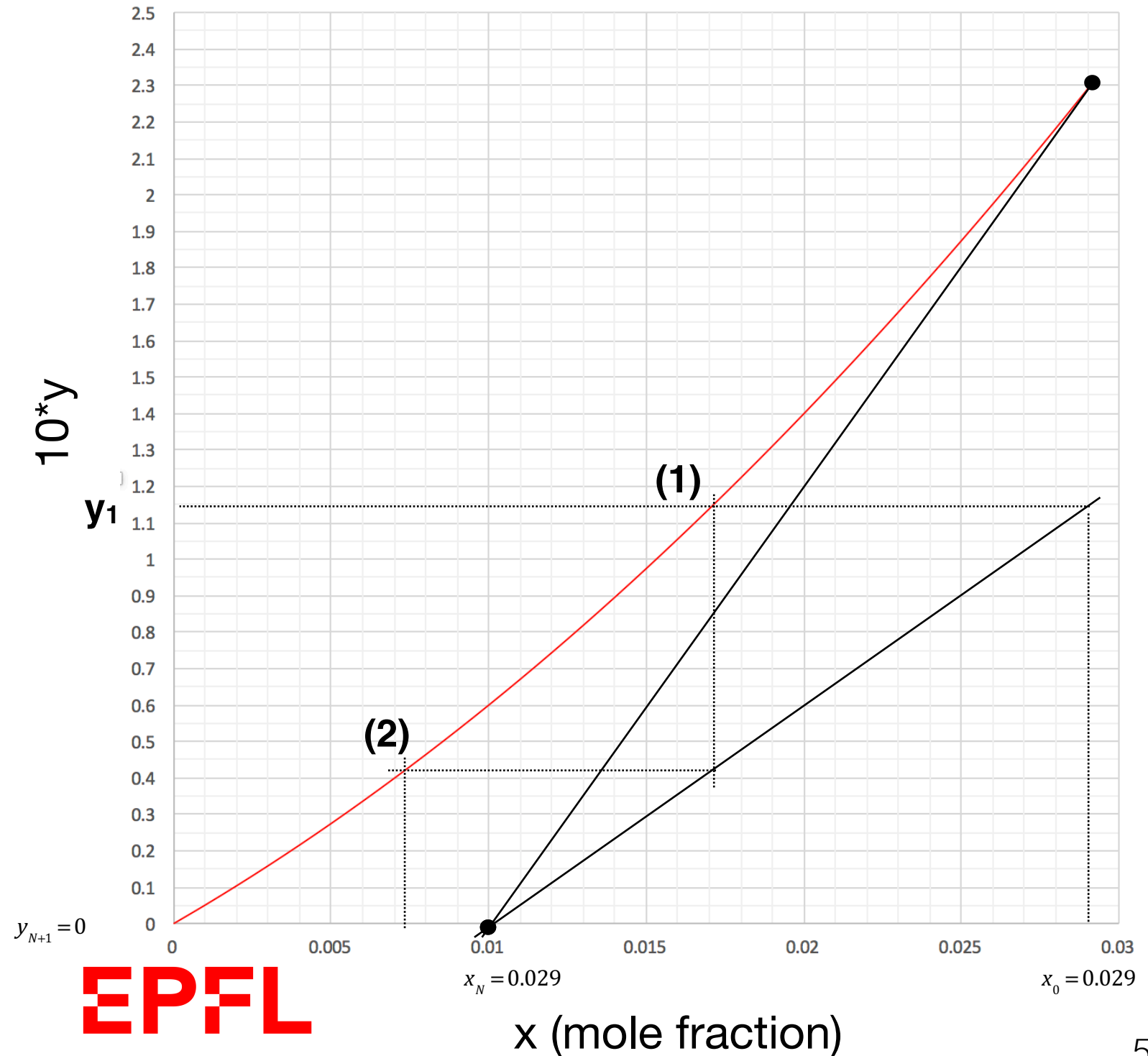


$$\frac{L}{G_{\min}} = \frac{2.3 - 0}{0.029 - 0.01} = \frac{2.3}{0.019} = 121$$

$$\frac{L}{G} = 0.5 * \frac{L}{G_{\min}} = 60.5$$

$$y_1 = \frac{1.15}{10} = 0.115$$

$$y_1 = 11.5\%$$



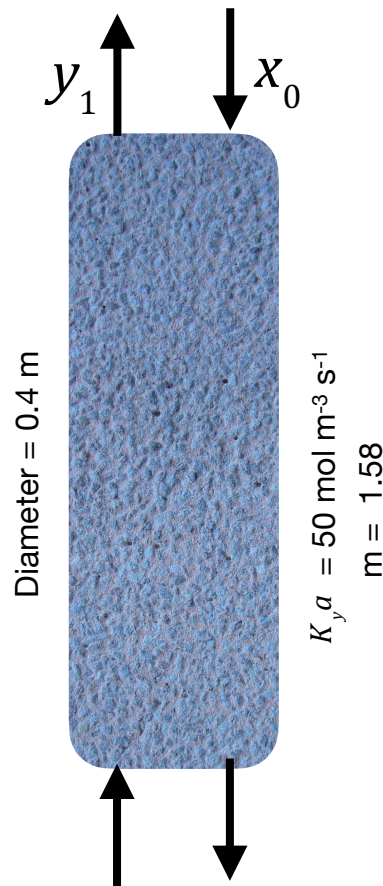
Solution to Exercise problem 2

Calculate HTU, NTU, and h for the following problem. How would you decrease HTU?

$$h = \frac{G}{K_y a A} \left[\left(\frac{1}{1 - \frac{mG}{L}} \right) \ln \left(\frac{y_{N+1} - mx_N}{y_1 - mx_0} \right) \right]$$

Flue gas
0.04% CO₂

Pure amine
4.8 mole/s



Flue gas, 2.3 mole/s
1.26% CO₂

$$y_{N+1} = 0.0126$$

$$y_1 = 0.0004$$

$$x_0 = 0$$

$$L(x_N - x_0) = G(y_{N+1} - y_1)$$

$$x_N = x_0 + \frac{G}{L}(y_{N+1} - y_1) = 0.0058$$

$$HTU = \frac{G}{K_y a A} = \frac{2.3}{50 * \pi * 0.2^2} = 0.37 \text{ meters}$$

$$NTU = \left(\frac{1}{1 - \frac{mG}{L}} \right) \ln \left(\frac{y_{N+1} - mx_N}{y_1 - mx_0} \right) = \left(\frac{1}{1 - \frac{1.58 * 2.3}{4.8}} \right) \ln \left(\frac{0.0126 - 1.58 * 0.0058}{0.0004 - 1.58 * 0} \right) = 8.85$$

$$h = HTU * NTU = 0.37 * 8.85 = 3.2 \text{ meters}$$

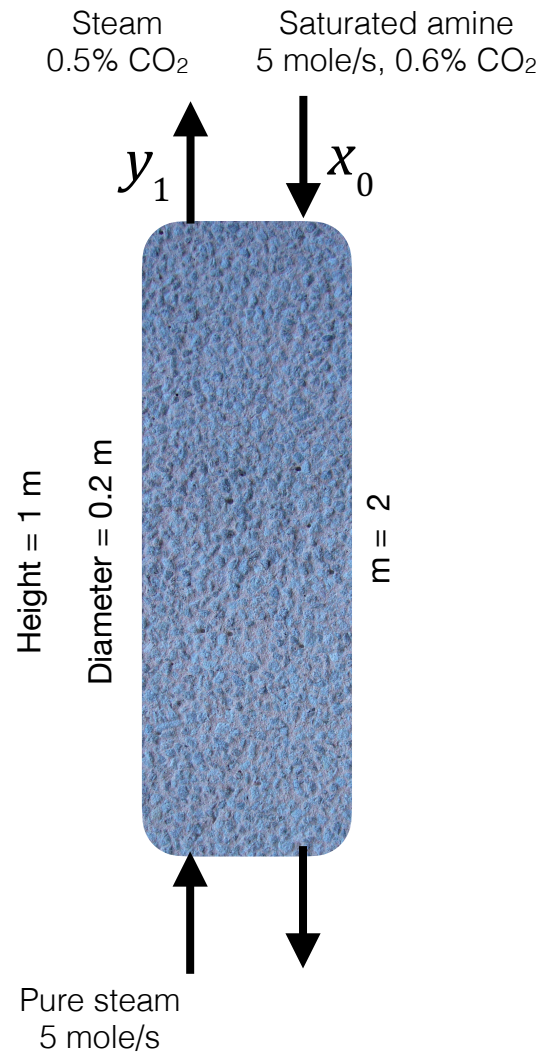
Bigger diameter column (larger A) will decrease HTU

Decreasing gas flow rate will decrease HTU

Solution to exercise problem 3

Calculate HTU, NTU, and $K_y a$ for the following problem.

$$h = \frac{G}{K_y a A} \left[\left(\frac{1}{1 - \frac{mG}{L}} \right) \ln \left(\frac{y_{N+1} - mx_N}{y_1 - mx_0} \right) \right]$$



$$y_{N+1} = 0$$

$$y_1 = 0.005$$

$$x_0 = 0.006$$

$$L(x_0 - x_N) = G(y_1 - y_{N+1})$$

$$x_N = x_0 - \frac{G}{L}(y_1 - y_{N+1}) = 0.001$$

$$NTU = \left(\frac{1}{1 - \frac{mG}{L}} \right) \ln \left(\frac{y_{N+1} - mx_N}{y_1 - mx_0} \right) = \left(\frac{1}{1 - \frac{2 \cdot 5}{5}} \right) \ln \left(\frac{0 - 2 \cdot 0.001}{0.005 - 2 \cdot 0.006} \right) = 1.25$$

$$HTU = \frac{h}{NTU} = \frac{1}{1.25} = 0.8$$

$$K_y a = \frac{5}{0.8 \cdot \pi \cdot 0.1^2} = 199.2 \text{ mole } m^{-3} s^{-1}$$